

Life cycle assessment modifications for understanding the effect of carbon dioxide transformations into high value-added products

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Abstract.

The increase in carbon dioxide (CO₂) emissions from industrial activities is a critical driver of climate change, requiring urgent mitigation strategies [1]. The largest industrial CO₂ emitters globally include power generation (coal and natural gas plants), cement production, steel manufacturing, and the chemical industry, which together account for a significant share of anthropogenic emissions [2]. These sectors rely on carbon-intensive processes, making decarbonization a complex challenge. In response, Carbon Capture and Storage (CCS) technologies have been widely explored as a mitigation strategy by capturing CO₂ and a further storage underground to prevent releasing into the atmosphere [3]. Nevertheless, CCS faces economic, technical, and long-term storage concerns, limiting the large-scale adoption. As an alternative, Carbon Capture and Utilization (CCU) technologies have gained attention by valorizing CO₂ as a raw material for the synthesis of fuels, chemicals, and other value-added products. This approach allows the promotion of a circular carbon economy and a decrease in dependence on fossil-based resources [4]. Nonetheless, as depicted by Müller et al. [5], the environmental feasibility of these CCU pathways must be critically assessed to determine whether they truly lead to net CO₂ reductions or merely result in delayed emissions, depending on process efficiency, energy sources, and system boundaries. Furthermore, CO₂-based products provide temporary carbon storage, delaying emissions and mitigating climate impact temporarily. Nevertheless, this benefit is realized only once; once conventional products are fully replaced, emission time profiles stabilize [6].

This study conducts a Life Cycle Assessment (LCA) of three CCU technologies, focusing on the potential to contribute to sustainable production systems. The first stand-alone case considered the synthesis of dimethyl carbonate (DMC), a versatile chemical used as a green solvent and precursor for polycarbonates, under supercritical CO₂ conditions by evaluating, through experimental test, different molar ratios of methanol, propylene glycol and K₂CO₃ for three temperatures (i.e., 60, 80, and 100 °C) [7]. The second stand-alone case evaluated the electrochemical reduction of CO₂ to formic acid, a key compound in hydrogen storage, fuel cells, and as a feedstock for the chemical industry, through the use of Sn-based electrodes and three different electrolytes (i.e., 0.1 M KHCO₃, 0.5M K₂SO₄, and 0.1M Na₂SO₄/Na₂CO₃) [8]. The third stand-alone case explored CO-rich syngas production via biomass gasification using CO₂ as a co-gasifying agent, a process to enable the synthesis of synthetic fuels, methanol, and other carbon-based chemicals. This last CO₂ upgrading alternative was evaluated according to the methodology presented by Shen et al. [9], considering sole-air gasification of corn cob and the influence on CO production when co-gasifying at a 15 vol.% CO₂ / 85 vol.% air ratio. Moreover, to deepen the analysis, this study proposed the integration of these three processing pathways, distributing the CO₂ flow based on market demand analysis to evaluate different production scenarios. Four configurations were assessed: i) production of CO-rich syngas and DMC, ii) formic acid and CO-rich syngas production, iii) production of DMC and formic acid, and iv) the combined production of DMC, formic acid, and CO-rich syngas. This approach aimed at understanding how routes integration affected the impact categories considered in the environmental

analysis, providing insights into the trade-offs and potential synergies between different CCU technologies. To enhance the accuracy of the environmental assessment, a modification of the conventional LCA methodology was implemented in the SimaPro software, integrating tailored process modeling, refined energy and material inventory adjustments, and scenario-based sensitivity analysis [5]. The workflow included defining system boundaries for all the scenarios, adapting impact allocation methods, updating energy source profiles, and applying the ReCiPe Midpoint (H) for reaching a comprehensive impact evaluation. Then, the system boundaries were established by a gate-to-gate analysis, referring to the stage of flue gas feed to the capture unit (through the chemical absorption process using monoethanolamine), up to the valorization of CO₂ in the final products. **Figure 1** presents the system boundaries considered for the environmental assessment of this study. The functional unit was defined as 1.0 kg_{CO₂} valorized in each scheme. Moreover, mass allocation methods was defined for the evaluated valorization routes.

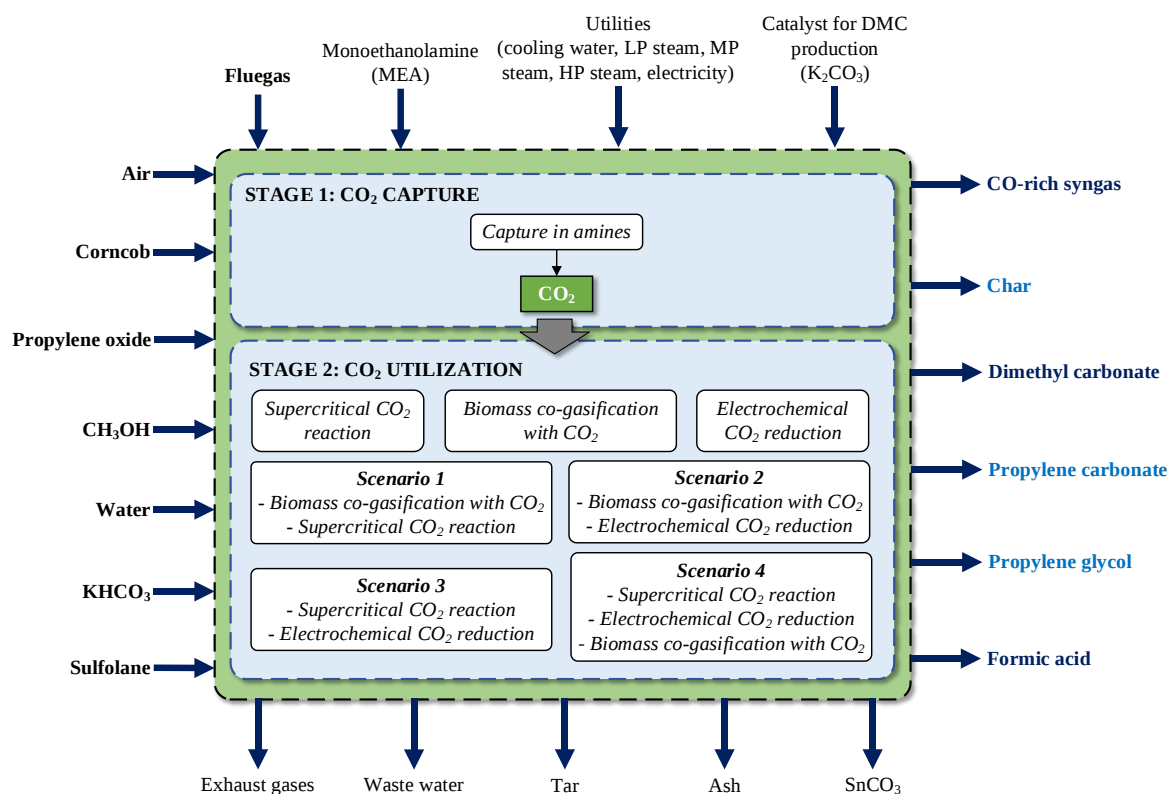


Figure 1. System boundary for environmental assessment of the proposed CCU schemes.

Under the mass allocation approach, CO₂ uptake was treated as negative emissions before eventually release. Moreover, an end-of-life (EoL) model, as positive emissions, was adopted to ensure CO₂ balance. Regarding the assumptions considered, infrastructure for compression, transportation, and distribution was neglected since CO₂ capture and chemical synthesis occurred on-site, with a 5% purge of outlet gases to prevent inert gas accumulation. Given the unique nature of CO₂ utilization in LCA, new indicators were needed beyond traditional carbon footprints and resource use, as CO₂ functions both as a waste product and a raw material. Results interpretation in these schemes is crucial to accurately assess climate benefits, as conventional indicators may not considered temporary storage, delayed emissions, and sequestration potential of CO₂-based products. Then, new tailored indicators were defined to ensure a more comprehensive evaluation of environmental trade-offs and long-term sustainability in CCU systems.

Among the stand-alone technologies analyzed, CO-rich syngas production proved to be the most environmentally promising, primarily due to the high yield (i.e., 44.74 wt. %) and validated CO₂ capture efficiency. Moreover, the biochar generated during the process enhances CO₂ sequestration, leading to a climate change impact value of 0.22 kg_{CO2-eq}/kg_{CO2-valorized}. Conversely, DMC production contributed significantly to environmental burdens due to the reliance on chemical precursors such as methanol and propylene oxide, resulting in an impact of 1.16 kg_{1,4-DB-eq}/kg_{CO2-valorized}. In the case of formic acid production, the low technological maturity and low yield (i.e., 14.57 wt. %) required high voltage inputs and frequent electrode regeneration due to surface precipitation and corrosion, leading to an aggravated impact of 0.59 kg_{CO2-eq}/kg_{CO2-valorized}. Finally, Scenario 1, where the integration of CO-rich syngas and DMC production was considered, was identified as the most promising among the proposed configurations. The use of more mature technologies in this scenario resulted in lower process mass and energy intensities, leading to more favorable environmental impact category values compared to the other integration scenarios. Thus, new indicators emerge to assess CO₂ utilization in CCU systems: i) CO₂ utilization efficiency, to differentiate between processes merely capturing CO₂ and those converting the gas into valuable products, ii) net carbon sequestration, to evaluate whether CO₂ utilization leads to long-term emission reductions or simply shifts emissions without contributing to overall sequestration, iii) recyclability of CO₂-derived products, to assess the potential of each product for reuse at the end of their life cycle, promoting a circular economy, iv) CO₂ recovery potential, to quantify the amount of CO₂ captured, utilized, or stored relative to total system emissions, reflecting the ability to close the carbon loop, v) CO₂ emissions avoidance, to measure the emissions prevented by using CO₂ as a feedstock instead of fossil-based resources, vi) CO₂ retention time, to determine how long the carbon remains stored before being released, and vii) CO₂ sequestration rate, to quantify the net amount of CO₂ permanently or temporarily sequestered both in geosphere or hydrosphere, as through photosynthesis. Finally, the techno-economic efficiency of CO₂ utilization was also considered as an additional indicator to integrate economic viability with environmental performance, balancing the costs of capture, conversion, and production with the value generated. Finally, through the normalization of results for CO₂ utilization, fair comparisons were ensured by accounting for temporary storage, delayed emissions, and system-specific impacts, enabling more accurate sustainability assessments.

This study highlighted the importance of LCA in evaluating CCU technologies, providing a comprehensive understanding of CO₂ utilization pathways and the potential environmental trade-offs. LCA demonstrated to be a crucial tool for identifying the most sustainable strategies by assessing the material, energy, and environmental implications of different CCU routes. By integrating LCA into the decision-making process, the enhancement of CO₂ valorization efficiency and the development of climate-mitigation technologies contributing to the reduction of greenhouse gas (GHG) emissions can be achieved.

Keywords: *Carbon Capture and Utilization; Life Cycle Assessment; Dimethyl carbonate (DMC) synthesis; Electrochemical CO₂ reduction; Biomass gasification with CO₂; Greenhouse Gas (GHG) mitigation.*

Acknowledgments.

This research work was funded within the framework of the research project “Aprovechamiento y valorización sostenible de residuos sólidos orgánicos y su posible aplicación en biorrefinerías y tecnologías de residuos a energía en el departamento de Sucre” code BPIN 2020000100189.

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